Amendments to the Claims:

This listing of claims will replace all prior versions and listings of the claims in the application:

Listing of the claims:

1. (Canceled)
2. (Canceled)
3. (Canceled)

4. (Currently Amended) A process for separating a VWF having a high specific VWF activity from a VWF having a low specific VWF activity, said process comprising the steps: (a) binding VWF to a hydroxylapatite column matrix, (b) washing out VWF having a specific VWF activity less than 70 U per mg VWF antigen **using a wash buffer containing 100 – 300 mM phosphate salt** and (c) eluting a VWF having a specific VWF activity greater than 120 U per mg VWF antigen **using an elution buffer containing 200 – 500 mM phosphate salt**.

5. (Previously Presented) The process according to claim 4, characterized in that the binding of step (a) is carried out at a pH between 5 and 7.

6. (Currently Amended) The process according to claim 4, characterized in that ~~a~~ **the phosphate salt is selected from the group consisting of** sodium **phosphate** ~~or~~ **and** potassium phosphate ~~containing solution is used as a running buffer~~.

7. (Canceled) ~~The process according to claim 4, wherein the washing of step (b) is performed using a wash buffer containing 100 – 300 mM sodium or potassium phosphate, and the elution of step (c) is performed using an elution buffer containing 200 – 500 mM sodium or potassium phosphate~~.

8. (Previously Presented) The process according to claim 4, wherein the VWF having a specific VWF activity greater than 120 U per mg VWF antigen eluted in step (c) is substantially free from fibrinogen and fibronectin.

9. (Previously Presented) The process according to claim 4, characterized in that the hydroxylapatite column matrix is a ceramic hydroxylapatite.

10. (Original) The process according to claim 9, characterized in that the ceramic hydroxylapatite is type I or type II.

11. (Previously Presented) The process according to claim 4, characterized in that a previously purified plasma fraction is used as a starting material.

12. (Previously Presented) The process according to claim 4, characterized in that a further purified cryoprecipitate solution is used as a starting material.

13. (Previously Presented) The process according to claim 4, characterized in that a cryoprecipitate solution precipitated with aluminum hydroxide is used as a starting material.

14. (Previously Presented) The process according to claim 4, characterized in that a chromatographically pre-purified cryoprecipitate solution precipitated with aluminum hydroxide is used as a starting material.

15. (Previously Presented) The process according to claim 4, further comprising the step of carrying out a pH precipitation prior to step (a) to separate fibronectin.

16. (Previously Presented) The process according to claim 4, characterized in that a protein solution with recombinantly produced VWF is used as a starting material.

17. (Previously Presented) The process according to claim 4, characterized in that the hydroxylapatite column matrix contains fluoride ions.

18. (Canceled)

19. (Canceled)

20. (Canceled)

21. (Canceled)

22. (Canceled)

23. (Canceled)

24. (Canceled)

25. (Canceled) ~~The process according to claim 4, wherein the washing of step (b) is performed at a salt concentration ranging from 100 – 300 mM and the elution of step (c) is performed at a salt concentration ranging from 200 – 500 mM.~~

26. (Currently Amended) The process according to claim 4, wherein the ~~washing of step (b) is performed at a~~ **wash buffer has a phosphate** salt concentration ranging from 200 – 300 mM and the ~~elution of step (c) is performed at a~~ **elution buffer has a phosphate** salt concentration ranging from 250 – 500 mM.

27. (Currently Amended) The process according to claim 4, wherein the ~~washing of step (b) is performed at a~~ **wash buffer has a phosphate** salt concentration ranging from 200 – 270 mM and the ~~elution of step (c) is performed at a~~ **elution buffer has a phosphate** salt concentration ranging from 300 – 400 mM.